

Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

1.-8. (Cancelled)

| ~~g.~~ (Currently Amended) A process for the continuous preparation of a silane of the formula I

$R^6R^5CH-R^4CH-SiR^1R^2R^3$ (I),

which comprises continuously reacting a silane of the formula II

$HSiR^1R^2R^3$ (II),

with an alkene of the formula III

$R^6R^5CH=CHR^4$ (III),

$R^6R^5C=CHR^4$ (III).

in the presence of an iridium compound of the formula IV as catalyst

$[(diene)IrCl]_2$ (IV),

and free diene as cocatalyst, where

R^1 , R^2 , R^3 are each a monovalent Si-C-bonded, unsubstituted or halogen-substituted C_1-C_{18} -hydrocarbon radical, a chlorine atom or a C_1-C_{18} -alkoxy radical,

R⁴, R⁵, R⁶ are each a hydrogen atom, a monovalent C₁-C₁₈-hydrocarbon radical optionally bearing one or more F, Cl, OR, NR'₂, CN or NCO substituents, a chlorine atom, a fluorine atom or a C₁-C₁₈-alkoxy radical, where 2 radicals R⁴, R⁵, R⁶ together with the carbon atoms to which they are bound may form a cyclic radical,

R is a hydrogen atom or a monovalent C₁-C₁₈-hydrocarbon radical and diene is a C₄-C₅₀-hydrocarbon compound optionally bearing one or more F, Cl, OR, NR₂, CN or NCO substituents and has at least two ethylenic C=C double bonds, with the reaction temperature being 30-200°C and the reaction pressure being 0.11-50.0 Mpa, in a mol ratio of alkene (III) to silane (II) such that 0.01 to 100 mol % of (III) is present in excess over (II) when said catalyst is present.

2 10. (Previously Presented) The process of claim 8, wherein R¹, R² and R³ are C₁-C₆-alkyl radicals, C₁-C₆-alkoxy radicals, or mixtures thereof.

3 11. (Previously Presented) The process of claim 9, wherein R⁵ and R⁶ are C₁-C₆-alkyl radicals, C₁-C₆-alkoxy radicals, or mixtures thereof.

4 12. (Previously Presented) The process of claim 9, wherein R⁴ is selected from the group consisting of hydrogen, methyl, and ethyl.

5 13. (Previously Presented) The process of claim 9, wherein free diene is added as cocatalyst in a concentration of from 1×10⁻⁶ to 1 mol%, based on the silane component of the formula II.

6 14. (Previously Presented) The process of claim 9, wherein the reaction temperature is 60-100°C.

7 15. (Previously Presented) The process of claim 9, wherein the catalyst of the formula IV is [(cycloocta-1c,5c-diene)IrCl]₂.

8 16. (Previously Presented) The process of claim 15, wherein the cocatalyst is 1,5-cyclooctadiene.

17. (Cancelled)

9 18. (Currently Amended) The process of claim 9, wherein the alkene of formula (III) is present in [[0.01]] 0.1 mol percent to [[100]] 10 mol percent stoichiometric excess relative to the silane of formula (II).

10 19. (Previously Presented) The process of claim 9, wherein reacting takes place in an aprotic solvent.

11 20. (Previously Presented) The process of claim 19, wherein the aprotic solvent comprises silane (I).

12 21. (Previously Presented) The process of claim 9, further comprising separating silane (I) and leaving a high boiling residue, and recycling at least a portion of the high boiling residue as catalyst to the step of reacting.

13 22. (Previously Presented) The process of claim 9 wherein the free diene is not the same as the diene of the catalyst (IV).